

WHAT IS CLAIMED IS:

1. A method of removing contamination from a Fischer-Tropsch derived hydrocarbon stream, the method comprising:
 - a) filtering a Fischer-Tropsch derived hydrocarbon stream to produce a filtered hydrocarbon stream;
 - b) passing the filtered hydrocarbon stream to at least one distillation step to remove contamination from the filtered hydrocarbon stream, the distillation step producing a distillate product stream and a bottoms fraction, wherein the contamination is substantially concentrated in the bottoms fraction; and
 - c) recovering the bottoms fraction from the distillation step, wherein the amount of the bottoms fraction is less than about 35 percent by volume of the filtered hydrocarbon stream.
- 15 2. The method of claim 1, wherein the amount of the bottoms fraction is less than about 15 percent by volume of the filtered hydrocarbon stream.
3. The method of claim 1, wherein the filtering step removes particulates having an average size greater than or equal to about 10 microns.
- 20 4. The method of claim 1, wherein the filtering step removes contamination having an average size greater than or equal to about 1 micron.
5. The method of claim 1, wherein the distillation step is carried out in a vacuum distillation column.
- 25 6. The method of claim 1, wherein the contamination is derived from a Fischer-Tropsch catalyst.

7. The method of claim 1, wherein the distillation step removes soluble contamination from the Fischer-Tropsch derived hydrocarbon stream, the soluble contamination being derived from a Fischer-Tropsch catalyst.
- 5 8. The method of claim 7, wherein the soluble contamination comprises a material selected from the group consisting of aluminum, cobalt, titanium and iron.
9. The method of claim 1, wherein at least about 70 percent by weight of the contamination present in the filtered hydrocarbon stream is isolated in the bottoms fraction.
- 10 10. The method of claim 1, wherein at least about 85 percent by weight of the contamination present in the filtered hydrocarbon stream is isolated in the bottoms fraction.
- 15 11. The method of claim 1, wherein the Fischer-Tropsch derived hydrocarbon stream is a C₃₊ product.
- 20 12. The method of claim 1, further including passing the distillate product stream to a hydroprocessing reactor having a hydroprocessing catalyst.
- 25 13. The method of claim 1, wherein the distillation step comprises a first distillation step and a second distillation step, the first distillation step producing a first overhead stream and a first bottoms stream, and wherein the second distillation step produces a second overhead stream and a second bottoms stream.
- 30 14. The method of claim 13, wherein the first overhead stream has a range of boiling points less than about 800 to 950°F, and the first bottoms stream has a range of boiling points greater than about 800 to 950°F.

15. The method of claim 13, wherein the first overhead stream is passed to the hydroprocessing reactor, and the first bottoms stream is passed to the second distillation step.
- 5 16. The method of claim 13, wherein the second distillation step comprises a vacuum distillation, and the second bottoms stream has an initial boiling point of greater than about 1000°F.
- 10 17. The method of claim 13, wherein the second overhead stream is passed to the hydroprocessing reactor.
18. The method of claim 13, wherein the second bottoms stream is less than about 15 percent by volume of the Fischer-Tropsch derived hydrocarbon stream.
- 15 19. The method of claim 13, further including the step of treating the second bottoms stream with a treatment selected from the group consisting of dispensing the second bottoms stream in crude oil, passing the second bottoms stream to a third distillation step, processing the second bottoms stream into a fuel, and recycling the second bottoms stream in a recycling operation.

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